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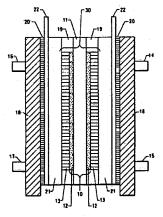
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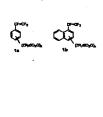
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(54) Title: STABLE TRIFLUOROSTYRENE CONTAINING COMPOUNDS GRAFTED TO BASE POLYMERS





(57) Abstract: A fluorinated ion exchange polymer prepared by grafting at least one grafting monomer on to at least one base polymer, wherein the grafting monomer comprises structure 1a or 1b: wherein Z comprises S, SO₂, or POR wherein R comprises a linear or branched perfluoroalkyl group of 1 to 14 carbon atoms optionally containing oxygen or chlorine, an alkyl group of 1 to 8 carbon atoms, an aryl group of 6 to 12 carbon atoms or a substituted aryl group of 6 to 12 carbon atoms; RF comprises a linear or branched perfluoroalkene group of 1 to 20 carbon atoms, optionally containing oxygen or chlorine; Q is chosen from F, -OM, NH₂, -N(M)SO₂R²_F, and C(M)(SO₂R²_F)₂, wherein M comprises H, an alkali cation, or ammonium; R²_F groups comprise alkyl of 1 to 14 carbon atoms which may optionally include ether oxygens or aryl of 6 to 12 carbon atoms where the alkyl or aryl groups may be perfluorinated or partially fluorinated; and n is 1 or 2 for 1a, and n is 1, 2, or 3 for 1b. These ion exchange polymers are useful in preparing catalyst coated membranes and membrane electrode assemblies used in fuel cells.

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

TITLE

STABLE TRIFLUOROSTYRENE CONTAINING COMPOUNDS GRAFTED TO BASE POLYMERS

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FIELD OF THE INVENTION

The present invention relates to a novel compound grafted to a base polymer, and its use in electrochemical cells as membranes, and more particularly to the use of these grafted polymers in fuel cells. This invention was made with government support under Contract No. DE-FC04-02AL67606 awarded by the U.S. Department of Energy. The government has certain rights in the invention.

BACKGROUND OF THE INVENTION

Electrochemical cells, such as fuel cells and lithium-ion batteries are known. Depending on the operating conditions, each type of cell places a particular set of requirements upon the electrolytes used in them. For fuel cells, this is typically dictated by the type of fuel, such as hydrogen or methanol, used to power the cell and the composition of the membrane used to separate the electrodes. Proton-exchange membrane fuel cells, powered by hydrogen as the fuel, could be run at higher operating temperatures than currently employed to take advantage of lower purity feed streams, improved electrode kinetics, better heat transfer from the fuel cell stack to improve its cooling. Waste heat is also employed in a useful fashion. However, if current fuel cells are to be operated at greater than 100 °C then they must be pressurized to maintain adequate hydration of typical proton-exchange membranes to support useful levels of proton conductivity.

There is an ongoing need to discover novel grafted films that improve the performance of the latest generation of electrochemical cells, such as fuel cells and lithium-ion batteries, to develop new membrane materials that will maintain adequate proton conductivity at lower levels of hydration and have sufficient durability for the intended application.

SUMMARY OF THE INVENTION

In a first aspect, the invention provides a fluorinated ion exchange polymer prepared by grafting at least one grafting monomer on to at least one base polymer, wherein the grafting monomer comprises structure 1a or 1b:

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wherein Z comprises S, SO₂, or POR wherein R comprises a linear or branched perfluoroalkyl group of 1 to 14 carbon atoms optionally containing oxygen or chlorine, an alkyl group of 1 to 8 carbon atoms, an aryl group of 6 to 12 carbon atoms or a substituted aryl group of 6 to 12 carbon atoms;

R_F comprises a linear or branched perfluoroalkene group of 1 to 20 carbon atoms, optionally containing oxygen or chlorine;

Q is chosen from F, -OM, -NH₂, -N(M)SO₂R²_F, and -C(M)(SO₂R²_F)₂, wherein M comprises H, an alkali cation, or ammonium;

 R^2_F groups comprise alkyl of 1 to 14 carbon atoms which may optionally include ether oxygens or aryl of 6 to 12 carbon atoms where the alkyl or aryl groups may be perfluorinated or partially fluorinated; and n is 1 or 2 for 1a, and n is 1, 2, or 3 for 1b.

In the first aspect, the invention also provides the at least one grafting monomer further comprising at least one co-monomer chosen from compounds containing single or multiple vinyl groups, such as divinyl benzene, triallyl cyanurate; at least one monomer having the structure 2 or 3; and mixtures thereof:

wherein Y comprises H; halogen such as Cl, Br, F or I; linear or branched alkyl or perfluoroalkyl groups, wherein the alkyl group comprises C1 to C10 carbon atoms; or a perfluoroalkyl group containing oxygen, chlorine or bromine, and wherein the alkyl group comprises C1 to C10 carbon atoms.

In a second aspect, the invention provides a grafting process for making the ionic polymer comprising:

(a) forming a monomer composition comprising at least one grafting monomer, in neat form, emulsion form, or solution form; wherein the grafting monomer comprises structure 1a or 1b:

wherein Z comprises S, SO₂, or POR wherein R comprises a linear or branched perfluoroalkyl group of 1 to 14 carbon atoms optionally containing oxygen or chlorine, an alkyl group of 1 to 8 carbon atoms, an aryl group of 6 to 12 carbon atoms or a substituted aryl group of 6 to 12 carbon atoms;

R_F comprises a linear or branched perfluoroalkene group of 1 to 20 carbon atoms, optionally containing oxygen or chlorine;

Q is chosen from F, -OM, -NH₂, -N(M)SO₂R²_F, and -C(M)(SO₂R²_{F)2}, wherein M comprises H, an alkali cation, or ammonium;

R²_F groups comprise alkyl of 1 to 14 carbon atoms which may optionally include ether oxygens or aryl of 6 to 12 carbon atoms where the alkyl or aryl groups may be perfluorinated or partially fluorinated; and n is 1 or 2 for 1a, and n is 1, 2, or 3 for 1b.

- (b) irradiating a base polymer with ionizing radiation; and
- (c) contacting at least one base polymer with the monomer composition from step (a), at a temperature of about 0 °C to about 120 °C for about 0.1 to about 500 hours. The steps (b) and (c) may be performed simultaneously or sequentially.

In the second aspect, the invention also provides the at least one grafting monomer further comprising at least one co-monomer chosen from compounds containing single or multiple vinyl groups, such as divinyl benzene, triallyl cyanurate; at least one monomer having the structure 2 or 3; and mixtures thereof:

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wherein Y comprises H; halogen such as Cl, Br, F or I; linear or branched alkyl or perfluoroalkyl groups, wherein the alkyl group comprises C1 to C10 carbon atoms; or a perfluoroalkyl group containing oxygen, chlorine or bromine, and wherein the alkyl group comprises C1 to C10 carbon atoms

In a third aspect, the invention provides a catalyst coated membrane comprising a polymer electrolyte membrane, wherein the polymer electrolyte membrane comprises a fluorinated ion exchange polymer prepared by grafting at least one grafting monomer on to a base polymer, wherein the grafting monomer comprises structure 1a or 1b:

wherein Z comprises S, SO₂, or POR wherein R comprises a linear or branched perfluoroalkyl group of 1 to 14 carbon atoms optionally containing oxygen or chlorine, an alkyl group of 1 to 8 carbon atoms, an aryl group of 6 to 12 carbon atoms or a substituted aryl group of 6 to 12 carbon atoms;

R_F comprises a linear or branched perfluoroalkene group of 1 to 20 carbon atoms, optionally containing oxygen or chlorine;

Q is chosen from F, -OM, -NH₂, -N(M)SO₂R²_F, and -C(M)(SO₂R²_F)₂, wherein M comprises H, an alkali cation, or ammonium;

R²_F groups comprise alkyl of 1 to 14 carbon atoms which may optionally include ether oxygens or aryl of 6 to 12 carbon atoms where the alkyl or aryl groups may be perfluorinated or partially fluorinated; and n is 1 or 2 for 1a, and n is 1, 2, or 3 for 1b.

Optionally, the at least one grafting monomer further comprises comonomer chosen from compounds containing single or multiple vinyl

groups, such as divinyl benzene, triallyl cyanurate; at least one monomer having the structure 2 or 3; and mixtures thereof:

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wherein Y comprises H; halogen such as Cl, Br, F or I; linear or branched alkyl or perfluoroalkyl groups, wherein the alkyl group comprises C1 to C10 carbon atoms; or a perfluoroalkyl group containing oxygen, chlorine or bromine, and wherein the alkyl group comprises C1 to C10 carbon atoms.

In a fourth aspect, the invention provides a membrane electrode assembly comprising a polymer electrolyte membrane, having a first surface and a second surface, wherein the polymer electrolyte membrane comprises a fluorinated ion exchange polymer prepared by grafting at least one grafting monomer on to at least one base polymer film, wherein the grafting monomer comprises structure 1a or 1b:

wherein Z comprises S, SO₂, or POR wherein R comprises a linear or branched perfluoroalkyl group of 1 to 14 carbon atoms optionally containing oxygen or chlorine, an alkyl group of 1 to 8 carbon atoms, an aryl group of 6 to 12 carbon atoms or a substituted aryl group of 6 to 12 carbon atoms;

R_F comprises a linear or branched perfluoroalkene group of 1 to 20 carbon atoms, optionally containing oxygen or chlorine;

Q is chosen from F, -OM, -NH₂, -N(M)SO₂R²_F, and -C(M)(SO₂R²_F)₂, wherein M comprises H, an alkali cation, or ammonium;

 R^2_F groups comprise alkyl of 1 to 14 carbon atoms which may optionally include ether oxygens or aryl of 6 to 12 carbon atoms where the alkyl or aryl groups may be perfluorinated or partially fluorinated; and n is 1 or 2 for 1a, and n is 1, 2, or 3 for 1b.

Optionally, the at least one grafting monomer further comprises at least one co-monomer chosen from compounds containing single or multiple vinyl groups, such as divinyl benzene, triallyl cyanurate; at least one monomer having the structure 2 or 3; and mixtures thereof:

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wherein Y comprises H; halogen such as Cl, Br, F or I; linear or branched alkyl or perfluoroalkyl groups, wherein the alkyl group comprises C1 to C10 carbon atoms; or a perfluoroalkyl group containing oxygen, chlorine or bromine, and wherein the alkyl group comprises C1 to C10 carbon atoms

In the fourth aspect, the membrane electrode assembly further comprises at least one electrode prepared from an electrocatalyst coating composition present on the first and second surfaces of the membrane. It also further comprises at least one gas diffusion backing. Alternately, the membrane electrode assembly further comprises at least one gas diffusion electrode present on the first and second surfaces of the membrane, wherein the gas diffusion electrode comprises a gas diffusion backing and an electrode prepared from an electrocatalyst containing composition.

In a fifth aspect, the invention provides an electrochemical cell, such as a fuel cell, comprising a membrane electrode assembly, wherein the membrane electrode assembly comprises a polymer electrolyte membrane, having a first surface and a second surface, wherein the polymer electrolyte membrane comprises a fluorinated ion exchange polymer prepared by grafting at least one grafting monomer on to at least one base polymer, wherein the grafting monomer comprises structure 1a or 1b:

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wherein Z comprises S, SO₂, or POR wherein R comprises a linear or branched perfluoroalkyl group of 1 to 14 carbon atoms optionally containing oxygen or chlorine, an alkyl group of 1 to 8 carbon atoms, an aryl group of 6 to 12 carbon atoms or a substituted aryl group of 6 to 12 carbon atoms;

R_F comprises a linear or branched perfluoroalkene group of 1 to 20 carbon atoms, optionally containing oxygen or chlorine;

Q is chosen from F, -OM, -NH₂, -N(M)SO₂R²_F, and -C(M)(SO₂R²_F)₂, wherein M comprises H, an alkali cation, or ammonium;

R²_F groups comprise alkyl of 1 to 14 carbon atoms which may optionally include ether oxygens or aryl of 6 to 12 carbon atoms where the alkyl or aryl groups may be perfluorinated or partially fluorinated; and

n is 1 or 2 for 1a, and n is 1, 2, or 3 for 1b.

Optionally, the at least one grafting monomer further comprises at least one co-monomer chosen from compounds containing single or multiple vinyl groups, such as divinyl benzene, triallyl cyanurate; at least one monomer having the structure 2 or 3; and mixtures thereof:

wherein Y comprises H; halogen such as Cl, Br, F or I; linear or branched alkyl or perfluoroalkyl groups, wherein the alkyl group comprises C1 to C10 carbon atoms; or a perfluoroalkyl group containing oxygen, chlorine or bromine, and wherein the alkyl group comprises C1 to C10 carbon atoms

In the fifth aspect, the fuel cell further comprises at least one electrode prepared from an electrocatalyst containing composition, e.g., an anode and a cathode, present on the first and second surfaces of the

polymer electrolyte membrane. It also further comprises at least one gas diffusion backing. Alternately, the membrane electrode assembly in the fuel cell further comprises at least one gas diffusion electrode present on the first and second surfaces of the membrane, wherein the gas diffusion electrode comprises a gas diffusion backing and an electrode prepared from an electrocatalyst containing composition.

In the fifth aspect, the fuel cell further comprises a means for delivering a fuel to the anode, a means for delivering oxygen to the cathode, a means for connecting the anode and cathode to an external electrical load, hydrogen or methanol in the liquid or gaseous state in contact with the

hydrogen or methanol in the liquid or gaseous state in contact with the anode, and oxygen in contact with the cathode. The fuel is in the liquid or vapor phase. Some suitable fuels include hydrogen; alcohols such as methanol and ethanol; ethers such as diethyl ether, etc.

BRIEF DESCRIPTION OF DRAWINGS

Figure 1 is a schematic illustration of a single cell assembly.

Figure 2 is a schematic illustration of the lower fixture of a four-electrode cell for in-plane conductivity measurement.

DETAILED DESCRIPTION OF THE INVENTION Fluorinated Ion Exchange Polymer:

The fluorinated ion exchange polymers of the invention are useful as polymer electrolyte membranes in fuel cells, chloralkali cells, batteries, electrolysis cells, ion exchange membranes, sensors, electrochemical capacitors, and modified electrodes.

Fluorinated Monomers:

The fluorinated ion exchange polymer is made by grafting at least one grafting monomer on to a base polymer, wherein the grafting monomer comprises structure **1a** or **1b**:

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wherein Z comprises S, SO₂, or POR wherein R comprises a linear or branched perfluoroalkyl group of 1 to 14 carbon atoms optionally containing oxygen or chlorine, an alkyl group of 1 to 8 carbon atoms, an

aryl group of 6 to 12 carbon atoms or a substituted aryl group of 6 to 12 carbon atoms;

R_F comprises a linear or branched perfluoroalkene group of 1 to 20 carbon atoms, optionally containing oxygen or chlorine;

Q is chosen from F, -OM, -NH₂, -N(M)SO₂R²_F, and -C(M)(SO₂R²_F)₂, wherein M comprises H, an alkali cation, or ammonium;

R²_F groups comprise alkyl of 1 to 14 carbon atoms which may optionally include ether oxygens or aryl of 6 to 12 carbon atoms where the alkyl or aryl groups may be perfluorinated or partially fluorinated; and

n is 1 or 2 for 1a, and n is 1, 2, or 3 for 1b. Some suitable perfluorinated alkylene groups R_F may be chosen from $(CF_2)_q$ wherein q=1 to 16, $(CF_2)_q OCF_2 CF_2$ wherein q=1 to 12, and $(CF_2 CF(CF_3)O)_q CF_2 CF_2$ wherein q=1 to 6. Typically R_F comprises $(CF_2)_q$ wherein q=1 to 4; $(CF_2)_q OCF_2 CF_2$ wherein q=1 to 4; and $(CF_2 CF(CF_3)O)_q CF_2 CF_2$ wherein q=1 to 2 . R^2_F groups typically are chosen from methyl, ethyl, propyl, butyl, and phenyl, each of which may be partially fluorinated or perfluorinated. More typically R^2_F groups are chosen from perfluoromethyl, perfluoroethyl, and perfluorophenyl. Typically the group Z linking R_F with the trifluorostyrene ring is S (sulfide linkage) or SO_2 (sulfone linkage). Typically n is 1.

Typically the monomers having sulfonyl fluoride groups are represented by the structure 1aF or 1bF:

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The sulfonyl fluoride groups may be converted to acid, metal salt, amide, or imide form, either before the grafting reaction or subsequent to the grafting reaction.

Synthesis of grafting monomers

BrC₆H₄SH was converted into the potassium salt by reacting with KOH in MeOH. After being dried in vacuum, the salt reacted with BrCF₂CF₂Br in DMSO to give BrC₆H₄SCF₂CF₂Br in high yield. Sulfination with Na₂S₂O₄ and then chlorination produced the corresponding fluorosulfonyl chloride, followed by fluorine-chlorine exchange to give the fluorosulfonyl fluoride BrC₆H₄SCF₂CF₂SO₂F.

Coupling reaction of $BrC_6H_4SCF_2CF_2SO_2F$ with CF_2 =CFZnX with Pd catalysis according to Burton's method (Burton et al, JOC 53, 2714, 1988) gave the coupled product 1a1, which could be protected with Br_2 and then oxidized to form the corresponding sulfone. Debromination of the sulfone with Zn gave monomer 1a2.

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Other monomers such as trifluorostyrene and 1,4-bis(trifluorostyrene) were made in similar fashion according to Burton's method. Alternatively, the monomers can be prepared by reaction of sodium or potassium salts of bromothiophenol with IR_FSO₂E, wherein E is a protecting group such as imidazol. The resulting product BrC₆H₄SR_FSO₂E undergoes a palladium catalyzed coupling reaction with CF₂=CFZnX to give the CF₂=CFC₆H₄SR_FSO₂E Co-Monomers:

The grafting monomers may optionally include co-monomers to improve the grafting process, or to improve properties such as strength or resistance to solvent swelling. Co-monomers may be introduced along with monomers having structures 1a or 1b during the grafting reaction. The co-monomers must be capable of co-polymerization with monomers 1a or 1b under free-radical conditions. Suitable crosslinking monomers comprise co-monomer chosen from compounds containing single or multiple vinyl groups, such as divinyl benzene, triallyl cyanurate; at least one monomer having the structure 2 or 3; and mixtures thereof:

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wherein Y comprises H; halogen such as Cl, Br, F or I; linear or branched alkyl or perfluoroalkyl groups, wherein the alkyl group comprises C1 to C10 carbon atoms; or a perfluoroalkyl group containing oxygen, chlorine or bromine, and wherein the alkyl group comprises C1 to C10 carbon atoms. Some suitable substituents Y are chosen from hydrogen, chlorine, fluorine, methyl, ethyl, methoxy, perfluoromethyl, perfluoroethyl, perfluorobutyl, perfluoromethoxy, and -CF₂CF(CF₃)OCF₂CF₃.

Base Polymer:

The base polymer to be used as the substrate for the grafting
reaction may be a homopolymer or comprised of several comonomers.
The base polymer is typically chosen so that it imparts desirable mechanical properties to the final grafted polymer, is stable to the irradiation used to activate the polymer for grafting, and is stable under the

conditions to which it is exposed during use. For separators or membranes it is desirable that the base polymer be present in the form of a film, though other shapes may be desired depending on the electrochemical use. Suitable materials may generally include homopolymers or copolymers of non-fluorinated, fluorinated, and perfluorinated monomers. Partially or completely fluorinated polymers often impart increased chemical stability and are more typical. Some typical base polymers may include poly(ethylene-tetrafluorethylenetermonomer (ETFE) that comprises a terpolymer of ethylene and tetrafluoroethylene (TFE), in the range of 35:65 to 65:35 (mole ratios) with 10 from 1 to 10 mole% of a termonomer, perfluorobutyl ethylene in the case of DuPont Tefzel®; ETFE copolymers also using other termonomers (Neoflon® ETFE); ECTFE that comprises a copolymer of ethylene and chlorotrifluoroethylene; FEP that comprises a copolymer of TFE and hexafluoropropylene (HFP), optionally containing a minor amount (1-3 15 mol%) of perfluoro(alkyl vinyl ether) (PAVE), usually perfluoro(propyl vinyl ether) (PPVE) or perfluoro(ethyl vinyl ether) (PEVE); PFA that comprises a copolymer of TFE and PAVE, wherein PAVE may be PPVE or PEVE; MFA that comprises a copolymer of TFE, PMVE, and PPVE; PTFE that comprises a homopolymer of TFE; modified PTFE, that contains up to 0.5 20 mol% of another monomer, usually a PAVE; PVF that comprises a polymer of vinyl fluoride (VF); PVDF that comprises a polymer of vinylidene fluoride (VF2); copolymers of VF2 and HFP which are sold under the trademarks KynarFlex® and Viton® A by Atofina and by DuPont, respectively; polyethylene and polypropylene. The term 25 "modified" distinguishes these polymers from copolymers of TFE. The modified PTFE polymers are, like PTFE, not melt processible.

Typically, the base polymer may be chosen from poly(ethylene-tetrafluoroethylene), poly(ethylene-tetrafluoroethylene-termonomer) (Tefzel®, Neoflon® ETFE); poly(tetrafluoroethylene-hexafluoropropylene) (Teflon® FEP); poly(tetrafluoroethylene-perfluorovinylether) (Teflon® PFA), polytetrafluoroethylene (Teflon® PTFE); poly(ethylene-chlorotrifluoroethylene); poly(vinyledene fluoride) (Kynar® or Solef®); and poly(vinylidenefluoride-hexafluoropropylene) (Kynar® Flex). More typically, the base polymer is chosen from poly(ethylene-tetrafluoroethylene-termonomer), poly(tetrafluoroethylene-

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hexafluoropropylene), poly(tetrafluoroethylene-perfluoropropylvinylether), and poly(vinyledene fluoride).

Processes for making grafted polymers and membranes:

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The fluorinated ion exchange polymer may be prepared by a grafting process comprising the steps of:

- (a) forming a monomer composition comprising at least one grafting monomer having structure **1a** or **1b**, along with optional co-monomers, in neat form, emulsion form, or solution form
- (b) irradiating a base polymer, typically in film form, with ionizing radiation
- (c) contacting the base polymer with the monomer composition from step (a), at a temperature of about 0 °C to about 120 °C for about 0.1 to about 500 hours. The steps (b) and (c) may be performed simultaneously or sequentially.

The monomers used in the grafting process are chosen from at least one grafting monomers having structure **1a** or **1b**, along with optional co-monomers, as described above under Fluorinated Ion Exchange Polymer. Base polymers suitable for the process of the second aspect generally may include homopolymers or copolymers of fluorinated or perfluorinated monomers. Partially or completely fluorinated polymers often impart increased chemical stability and are typical. Typically, the base polymer may be chosen from those listed earlier.

Free radicals may be created in the base polymer in order to produce attachment sites for the grafting monomers using radiation. When the base polymer is in film form, the films are known as irradiated films. The radiation dosage should be sufficient to allow for the desired graft level to be reached, but not so high as to cause excessive radiation damage. Graft level is defined as (wt. of grafted polymer – wt. of base polymer)/(wt. of base polymer). The radiation may be provided in the form of electron beam, gamma ray, or X-rays. Electron beam irradiation is typically performed at a high dose rate that may be advantageous for commercial production. The irradiation may be done while the base polymer is in contact with the grafting monomers (simultaneous irradiation and grafting). However, if the free radicals of the base polymer are sufficiently stable, then the irradiation may be performed first and in a subsequent step the base polymer may be brought into contact with the grafting monomers (post-irradiation grafting). Base polymers suitable for

the post-irradiation grafting method are usually fluorinated polymers. In this case the irradiation may typically be done at sub-ambient temperatures, for example with base polymer cooled with dry ice, and it may be stored at a sufficiently low temperature to prevent decay of the free radicals prior to its use in the grafting reaction.

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With some substrates, such as poly(ethylene-tetrafluoroethylene) the irradiation may be performed in the presence of oxygen or in an oxygen-free environment, and an appreciable graft level can be obtained in either case. Typically grafting may be performed in an inert gas, such as nitrogen or argon. This may be accomplished by loading the base polymer films, within an inert-atmosphere box, into oxygen-barrier bags, sealing them shut (with or without grafting monomers and solvent), and then irradiating. In the case of post-irradiation grafting, the base polymer may then also be stored in the oxygen-free environment before and during the grafting reaction.

The grafting reaction may be performed by exposing the base polymer to a monomer composition containing the grafting monomers. In the simplest form, the neat liquid monomers may be used as the monomer composition. It is generally desirable to lower the quantity of fluorinated monomer used in the grafting reaction, and this may be accomplished by diluting it by forming an emulsion or a solution with a solvent, which thus increases the total working volume of the monomer composition. The monomer composition may thus be an emulsion made by mechanical or ultrasonic mixing of the monomers with water and/or alcohols such as isopropanol, and fluorinated or non-fluorinated surfactants such as fluorinated carboxylic salts, typically ammonium perfluorooctanoate and ammonium fluorooctanesulfonate. A third useful form for the monomer composition is a solution of the monomers in an inert organic solvent. Typical solvents include toluene, benzene, halobenzenes, fluorocarbons such as perfluoroethers, fluorochlorocarbons such as 1,1,2trichlorotrfluoroethane, chlorocarbons such as CH2Cl2, CH2ClCH2Cl, and hydrocarbons. The process for making grafted polymers by solvent grafting may also use fluoroalkyl benzene solvents. Preferred fluoroalkyl benzene solvents are trifluoromethylbenzene (α,α,α -trifluorotoluene), 1,3-bis(trifluoromethyl)benzene, and 1,4-bis(trifluoromethyl)benzene, and (pentafluoroethyl)benzene, with trifluoromethylbenzene being most preferred. We have found that aromatic compounds substituted with

fluorinated aliphatic groups, when used as solvents for the fluorinated vinyl monomers, provide fast rates for grafting monomers to fluorinated base polymers. The grafting solution may comprise mixtures of the grafting monomer(s) and the solvent, where the mole fraction of the solvent in the mixture is between 1% and 99%, more typically between 5% and 90%. Grafting may be accomplished by contacting the base polymer films, during irradiation or subsequent to irradiation, with the monomer composition and holding films at about 0 °C to about 120 °C for about 0.1 to about 500 hours. Typical temperatures are about 25 °C to about 100 °C, more typically about 35 to about 90 °C, and most typically about 40 to about 80 °C. Typical times are about 10 min to about 300 hours, more typically about 1 hour to about 200 hours, and most typically about 1 hour to about 100 hours. Subsequent to the grafting reaction, the solvent and unreacted monomer may be removed by extraction with a low-boiling solvent or through vaporization. The grafted polymer may also be extracted with a solvent in order to remove any polymer formed in the film that is not grafted to the base film.

Preparation of Ionic Polymers:

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This invention provides for the facile conversion of the fluorosulfonyl fluorides to acid form, without the use of sulfonation reagents. Polymers grafted with the monomers bearing pendant sulfonyl fluoride groups may be hydrolyzed with bases such as MOH or M₂CO₃ (M = Li, Na, K, Cs, NH₄) or MOH in MeOH and/or DMSO, and water. The hydrolysis may usually be carried out at room temperature to about 100°C, typically at room temperature to about 80°C. With polymeric substrates such as PVDF that are sensitive to strong base, it is preferable to use the weaker carbonate bases that avoid decomposition of the substrate. Treatment of polymeric salts with acids such as HNO₃ gave polymeric acids. It has been found that the particular linkage groups Z used here give rise to increased thermal stability of the ion exchange polymers that are in acid form.

The grafted polymers sulfide (Z = S) may be oxidized to sulfone polymers ($Z = SO_2$) using CrO_3 or hydrogen peroxide. Electrochemical Cell:

As shown in Figure 1, an electrochemical cell, such as a fuel cell, comprises a catalyst-coated membrane (CCM) (10) in combination with at least one gas diffusion backing (GDB) (13) to form an unconsolidated

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membrane electrode assembly (MEA). The catalyst-coated membrane (10) comprises a polymer electrolyte membrane (11) discussed above and catalyst layers or electrodes (12) formed from an electrocatalyst coating composition. The fuel cell may be further provided with an inlet (14) for fuel, such as hydrogen; liquid or gaseous alcohols, e.g. methanol and ethanol; or ethers, e.g. diethyl ether, etc., an anode outlet (15), a cathode gas inlet (16), a cathode gas outlet (17), aluminum end blocks (18) tied together with tie rods (not shown), a gasket for sealing (19), an electrically insulating layer (20), graphite current collector blocks with flow fields for gas distribution (21), and gold plated current collectors (22).

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Alternately, gas diffusion electrodes comprising a gas diffusion backing having a layer of an electrocatalyst coating composition thereon may be brought into contact with a solid polymer electrolyte membrane to form the MEA.

The electrocatalyst coating compositions used to apply the catalyst layers as electrodes on the CCM (10) or the GDE comprise a combination of catalysts and binders dispersed in suitable solvents for the binders, and may include other materials to improve electrical conductivity, adhesion, and durability. The catalysts may be unsupported or supported, typically on carbon, and may differ in composition depending on their use as anodes or cathodes. The binders may typically consist of the same polymer used to form the polymer electrolyte membrane (11), but may contain in part or be solely composed of other suitable polymer electrolytes as needed to improve the operation of the fuel cell. Some 25 examples include Nafion® perfluorosulfonic acid, sulfonated polyether sulfones, or their membranes.

The fuel cell utilizes a fuel source that may be in the gas or liquid phase, and may comprise hydrogen, an alcohol, or an ether. The fuel is humidified to the degree required to maintain adequate ionic conductivity in the solid polymer electrolyte membrane discussed above so that the fuel cell provides a high power output. Depending on the operating temperature, the fuel cell may be operated at elevated pressures to maintain the required degree of humidification. Typically a gaseous humidified hydrogen feed or methanol/water solution may be supplied to the anode compartment, and air or oxygen supplied to the cathode compartment.

Catalyst Coated Membrane:

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A variety of techniques are known for CCM manufacture, which apply an electrocatalyst coating composition similar to that described above onto a solid polymer electrolyte membrane. Some known methods include spraying, painting, patch coating and screen, decal, pad or flexographic printing.

In one embodiment of the invention, the MEA (30), shown in Figure 1, may be prepared by thermally consolidating the gas diffusion backing (GDB) with a CCM at a temperature of under about 200 °C, typically about 140 to about 160 °C. The CCM may be made of any type known in the art. In this embodiment, an MEA comprises a solid polymer electrolyte (SPE) membrane with a thin catalyst-binder layer disposed thereon. The catalyst may be supported (typically on carbon) or unsupported. In one method of preparation, a catalyst film is prepared as a decal by spreading the electrocatalyst coating composition on a flat release substrate such as Kapton® polyimide film (available from the DuPont Company). After the coating dries, the decal is transferred to the surface of the SPE membrane by the application of pressure and heat, followed by removal of the release substrate to form a catalyst coated membrane (CCM) with a catalyst layer having a controlled thickness and catalyst distribution. Alternatively, the catalyst layer is applied directly to the membrane, such as by printing, and the catalyst film is then dried at a temperature not greater than about 200°C.

The CCM, thus formed, is then combined with a GDB to form the MEA (30). The MEA is formed, by layering the CCM and the GDB, followed by consolidating the entire structure in a single step by heating to a temperature no greater than about 200 °C, typically in the range of about 140 to about 160 °C, and applying pressure. Both sides of the MEA can be formed in the same manner and simultaneously. Also, the composition of the catalyst layer and GDB may be different on opposite sides of the membrane.

The invention is illustrated in the following examples.

EXAMPLES

In-Plane Conductivity Measurement

The in-plane conductivity of membranes was measured under conditions of controlled relative humidity and temperature by a technique in which the current flowed parallel to the plane of the membrane. A four-

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electrode technique was used similar to that described in an article entitled "Proton Conductivity of Nafion® 117 As Measured by a Four-Electrode AC Impedance Method" by Y. Sone et al., J. Electrochem. Soc., 143,1254 (1996) that is herein incorporated by reference. Referring to Figure 2, a lower fixture (40) was machined from annealed glass-fiber reinforced Poly Ether Ether Ketone (PEEK) to have four parallel ridges (41) containing grooves that supported and held four 0.25 mm diameter platinum wire electrodes. The distance between the two outer electrodes was 25 mm, while the distance between the two inner electrodes was 10 mm. A strip of membrane was cut to a width between 10 and 15 mm and a length sufficient to cover and extend slightly beyond the outer electrodes, and placed on top of the platinum electrodes. An upper fixture (not shown), which had ridges corresponding in position to those of the bottom fixture, was placed on top and the two fixtures were clamped together so as to push the membrane into contact with the platinum electrodes. The fixture containing the membrane was placed inside a small pressure vessel (pressure filter housing), which was placed inside a forced-convection thermostated oven for heating. The temperature within the vessel was measured by means of a thermocouple. Water was fed from a calibrated Waters 515 HPLC pump (Waters Corporation, Milford, MA) and combined with dry air fed from a calibrated mass flow controller (200 sccm maximum) to evaporate the water within a coil of 1.6 mm diameter stainless steel tubing inside the oven. The resulting humidified air was fed into the inlet of the pressure vessel. The total pressure within the vessel (100 to 345 kPa) was adjusted by means of a pressure-control letdown valve on the outlet and measured using a capacitance manometer (Model 280E, Setra Systems, Inc., Boxborough, MA). The relative humidity was calculated assuming ideal gas behavior using tables of the vapor pressure of liquid water as a function of temperature, the gas composition from the two flow rates, the vessel temperature, and the total pressure. Referring to Figure 2, the slots (42) in the lower and upper parts of the fixture allowed access of humidified air to the membrane for rapid equilibration with water vapor. Current was applied between the outer two electrodes while the resultant voltage was measured between the inner two electrodes. The real part of the AC impedance (resistance) between the inner two electrodes, R, was measured at a frequency of 1 kHz using a potentiostat/frequency response analyzer (PC4/750™ with EIS software,

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Gamry Instruments, Warminster, PA). The conductivity, κ , of the membrane was then calculated as

 $\kappa = 1.00 \text{ cm} / (R \times t \times w),$

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where t was the thickness of the membrane and w was its width (both in cm).

Example 1: Irradiated Films

ETFE films were obtained in thicknesses of 30 μm and 55 μm (Tefzel® LZ5100 and LZ5200, DuPont Company, Wilmington, DE). PVdF films were obtained with a thickness 50 μm (Kynar® Goodfellow Corp. Berwyn, PA). The films were degassed and brought into a nitrogen-filled glove box. They were cut to size and sealed inside gas-barrier bags (PPD aluminum-foil-barrier bags from Shield Pack, Inc., West Monroe, LA). Dry ice pellets were placed in a metal tray for cooling and the bags with films were placed into the metal tray. The films were irradiated using an electron beam accelerator using 1 MV and a current of 2.2 mA. Up to 6 films were placed in each bag, and the bags were stacked up to 2 high in the tray. The beam was electronically scanned across a 40" aperture while the metal tray was moved slowly beneath the beam at a speed of 2.39 cm/s. Each pass resulted in a dosage of 20 kGy, and from 1 to 13 passes were used resulting in total dosages between 20 and 260 kGy. For dosages above 190 kGy, the passes were broken in to two groups with the inclusion of a three-minute pause between the groups to allow the 25 bags to cool. The irradiated films were stored in the bags under dry ice or in a refrigerator cooled to -40 °C.

Example 2:

Irradiated films from Example 1 were weighed and placed inside a glass reactor inside a dry box filled with nitrogen. The glass reactor was formed from two concentric glass tubes joined at the bottom to provide a thin annular volume, which was filled with the grafting solution. A deoxygenated solution of sulfide monomer CF₂=CF-C₆H₄S(CF₂)₂SO₂F, or sulfone monomer $CF_2=CF-C_6H_4S(CF_2)_2SO_2F$, and α,α,α -trifluorotoluene (TFT) (1:1 vol monomer:vol TFT) was poured over the films. The reactor was sealed with a septum and removed from the glove box. It was heated in an oil bath at the temperatures and for the times indicated in Table 1. The films were removed from the monomer solution and rinsed briefly with

 α,α,α -trifluorotoluene. The films were then heated in tetrahydrofuran (THF) at 70 °C for 4 hours to further remove residual solvent, monomer, and/or polymer that was not bonded to the base film. The films were dried under ambient conditions in a fume hood, reweighed. Graft Levels are indicated in Table 1. Graft Level was calculated as $(w_g-w)/w$, where w is the initial weight of the substrate film and w_g is the weight of the dried grafted film after the THF extraction.

In some cases the films were hydrolyzed by immersion in 10% KOH in $H_2O:MeOH:DMSO$ (5:4:1 wt:wt:wt) @ 50 °C for 16 hours. The films were acidified in 14% nitric acid at 50 °C for 1 hour, and then rinsed three times in deionized water at 50 °C for 15 minutes, changing to fresh water each time. Conductivities at 120 °C and 25, 50, or 95% RH are indicated in Table 1.

15 **Table 1**

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Exam- ple	Thick- ness (um)	Dose (kGy)	Monomer	Solvent	•	Graft Time (hr)	Graft Level (%)	Conduc- tivity 120C 25% RH	Conduc- tivity 120C 50% RH	Conduc- tivity 120C 25% RH
2a	30	200	sulfide	TFT	70	90	74	2.1	5.7	80
2b	30	140	sulfide	TFT	70	93	27			
2c	30	140	sulfide	IPA/H2O	70	70	40			
2d	55	140	sulfide	TFT	70	90	82			
2e	30	200	sulfide	TFT	60	93	68	1	. 2.6	45
2f	30	260	sulfide	TFT	60	93	206	14	56	380
2g	30	200	sulfone	TFT	70	90	32			1

Example 3: Emulsion Grafting

A 30 mL bottle fitted with a stirring bar was charged with 20 mL of deionized water and 4.0 mL of 20% ammonium perfluorooctanoate (C8) solution. The solution was bubbled with N_2 for 10 min., and 3.0 g of CF_2 = $CFC_6H_4SCF_2CF_2SO_2F$ were added. The resulting mixture was ultrasonicated for 3 min to give a milky emulsion.

Four films totaling 0.380 g from Example 1 irradiated with 140 kGy dosage were weighed and placed inside 30 mL bottle with a stirring bar inside a dry box filled with nitrogen. The emulsion made above was transferred into the sealed film-containing bottle via a cannula and then the emulsion was stirred at 60 °C for 3 days. The films were removed from the bottle and washed with MeOH, acetone and water. After the grafted films were dried in a vacuum oven at 60 °C with nitrogen bleed for 2 hrs, 1.176

g of grafted films were obtained with a 209.5% graft level. Graft level was calculated as (w_g-w)/w, where w is the initial weight of the film and w_g is the weight of the dried washed grafted film.

Example 4: Hydrolysis of Grafted Films

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Two grafted films (209% graft level) made in Example 3 were immersed in 10% KOH in H2O:MeOH:DMSO (5:4:1 wt:wt:wt) at 60 °C for 24 hours. The films were acidified in 10% nitric acid at 60 °C for 60 hrs, then rinsed with deionized water to neutral pH. The hydrolyzed film was swollen to 58 µm thickness. The conductivity of the sample was 10 measured in-plane at 80 °C under controlled humidity, varying from 25% first to 95% at the end. The conductivity values are given in the Table 2 below

Table 2

Temperature (oC)	RH (%)	Conductivity (mS/cm)
80	25	12
80	50	52.7
80	95	231.7

15 **Example 5: Emulsion Grafting**

A 30 mL, bottle fitted with a stirring bar was charged with 20 mL of deionized water and 4.0 mL of 20% ammonium perfluorooctanoate (C8) solution. The solution was bubbled with N₂ for 10 min. 3.0 q of CF₂=CFC₆H₄SCF₂CF₂SO₂F and 0.3 g of 1,4-di(trifluorovonyl)benzene were added. The resulting mixture was ultrasonicated for 3 min to give a milky emulsion.

Four films from Example 1, each weighing 0.266 g, irradiated with 140 kGy dosage were weighed and placed inside a 30 mL bottle with a stirring bar and placed inside a dry box filled with nitrogen. The emulsion 25 made above was transferred into the sealed film-containing bottle via a cannula and then the emulsion was stirred at 55 °C for 3 days. The films were removed from the bottle and washed with MeOH, acetone and water. After the grafted films were dried in a vacuum oven at 60°C with nitrogen bleed for 2 hours, 0.366 g of grafted films were obtained. A 37.6% graft level was calculated using the formula: (w₀-w)/w, where w is the initial weight of the film and wa is the weight of the dried grafted film

Example 6 Neat Grafting

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Four films from Example 1, each weighing 0.078~g, irradiated with 140 kGy dosage were immersed in neat CF_2 = $CFC_6H_4SCF_2CF_2SO_2F$ in a small tube at $60^{\circ}C$ for 3 days. The films were removed from the bottle and washed with MeOH, acetone and water. After the grafted films were dried in a vacuum oven at $60^{\circ}C$ with nitrogen bleed for 2 hrs, 0.134~g of grafted films were obtained. 71.8% Graft level was calculated using the formula: $(w_g-w)/w$, where w is A the initial weight of the film and w_g is the weight of the dried grafted film

10. Example 7. Hydrolysis and Conductivity

A grafted 1 mil ETFE film having 71.8% weight gain made in Example 6 was immersed in 10 wt% KOH in a solution of H₂O: MeOH: DMSO in a ratio of 5:4:1 (wt ratio) in a Petri dish @ 50 °C overnight. The film was rinsed in deionized water for 5 minutes at ambient temperature. The film was ion-exchanged to acid form by dipping in 10% nitric acid at 60 °C for 60 hrs, followed by rinsing in deionized water and then three

successive soaks in deionized water for 15 minutes at room temperature. The hydrolyzed film was swollen to 38µm thickness. The conductivity of the sample was measured in-plane at 80 °C under controlled humidity,

20 varying from 25% first to 95% at the end. The conductivity values are given in the Table 3 below:

Table 3

RH %	Conductivity (mS/cm)			
25	11.4			
50	49.0			
95	197.4			

25 The thermal stability of the membrane was evaluated using ASTM E1641-99 Standard Test Method for Decomposition Kinetics by Thermogravimetry, with the following exceptions: Air humidified at ambient temperature was used to flow through the sample chamber of a TGA (TA Instruments, New Castle, DE). The sample was heated to150 °C and held there for 2 hours during which time much of the water of hydration was lost. The temperature ramps were begun from 150 °C, using heating rates of 1, 3, 5, and 10 °C/min, and analyzing only the first stage of decomposition. The kinetic TGA study indicated that the

calculated time for completion of 10% of the first stage of decomposition at 120 $^{\circ}$ C was 200 hours.

Example 8 Oxidation of grafted membrane

A membrane made in example 4 was immersed in 3.0 g of CrO₃ in 50 mL CH₃CO₂H at 60 °C for 24 hrs. The film was removed and washed with water and then immersed in 100 mL of 10% HNO₃ at 60 °C for 24 hrs. The clear film was washed with water and immersed in 15% HNO₃ again at 60 °C for 24 hrs. The film was washed with water to neutral pH. The hydrolyzed film was swollen to 38µm thickness. The conductivity of the sample was measured in-plane at 80 °C under controlled humidity, varying from 25% first to 95% at the end. The conductivity values are given in the Table 4 below.

Table 4

Temperature (°C)	RH (%)	Conductivity (mS/cm)		
80	25	13.2		
80	50	53.1		
80	95	347.7		

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The kinetic TGA study using ASTM E1641-99 as modified above indicated that the calculated time for completion of 10% of the first stage of decomposition at 120 °C was 1.4x10⁸ hours.

CLAIMS

What is claimed is:

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1. A fluorinated ion exchange polymer prepared by grafting at least one grafting monomer on to at least one base polymer, wherein the grafting monomer comprises structure 1a or 1b:

wherein Z comprises S, SO₂, or POR wherein R comprises a linear or branched perfluoroalkyl group of 1 to 14 carbon atoms optionally containing oxygen or chlorine, an alkyl group of 1 to 8 carbon atoms, an aryl group of 6 to 12 carbon atoms or a substituted aryl group of 6 to 12 carbon atoms;

R_F comprises a linear or branched perfluoroalkene group of 1 to 20 carbon atoms, optionally containing oxygen or chlorine;

Q is chosen from F, -OM, -NH₂, -N(M)SO₂R²_F, and -C(M)(SO₂R²_F)₂, wherein M comprises H, an alkali cation, or ammonium;

 R^2_F groups comprise alkyl of 1 to 14 carbon atoms which may optionally include ether oxygens or aryl of 6 to 12 carbon atoms where the alkyl or aryl groups may be perfluorinated or partially fluorinated; and n.is 1 or 2 for 1a, and n is 1, 2, or 3 for 1b.

- 2. The fluorinated ion exchange polymer of Claim 1 wherein Q comprises fluorine.
- 3. The fluorinated ion exchange polymer of Claim 1 wherein R_F is chosen from (CF₂)_q wherein q = 1 to 16, (CF₂)_qOCF₂CF₂ wherein q = 1 to 12, and (CF₂CF(CF₃)O)_qCF₂CF₂ wherein q = 1 to 6, and R²_F is chosen from methyl, ethyl, propyl, butyl, and phenyl, each of which may be partially fluorinated or perfluorinated.
 - 4. The fluorinated ion exchange polymer of Claim 3 wherein R_F is chosen from $(CF_2)_q$ wherein q = 1 to 4; $(CF_2)_q OCF_2 CF_2$ wherein q = 1 to 4; and $(CF_2 CF(CF_3)O)_q CF_2 CF_2$ wherein q = 1 to 2, and R^2_F is chosen from perfluoromethyl, perfluoroethyl, and perfluorophenyl.

5. The fluorinated ion exchange polymer of Claim 3 wherein n = 1 and Z is S or SO₂.

6. The fluorinated ion exchange polymer of Claim 1 wherein the at least one grafting monomer further comprises at least one co-monomer chosen from compounds containing single or multiple vinyl groups; at least one monomer having the structure 2 or 3; and mixtures thereof:

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wherein Y comprises H; halogen such as Cl, Br, F or I; linear or branched alkyl or perfluoroalkyl groups, wherein the alkyl group comprises C1 to C10 carbon atoms; or a perfluoroalkyl group containing oxygen, chlorine or bromine, and wherein the alkyl group comprises C1 to C10 carbon atoms

7. The fluorinated ion exchange polymer of Claim 6 wherein the compounds containing single or multiple vinyl groups comprise bis(trifluorovinyl)-benzenes of structure 2 or triallyl cyanurate.

8. The fluorinated ion exchange polymer of Claim 7 wherein the substituents Y on co-monomer of structure 3 are chosen from hydrogen, chlorine, fluorine, methyl, ethyl, methoxy, perfluoromethyl, perfluoromethyl, perfluoromethoxy, and -CF₂CF(CF₃)OCF₂CF₃.

9. The fluorinated ion exchange polymer of Claim 1 wherein the base polymer comprises at least one homopolymer or copolymer prepared from non-fluorinated, fluorinated, or perfluorinated monomers.

10. The fluorinated ion exchange polymer of Claim 9 wherein the
25 base polymer is chosen from poly(ethylene-tetrafluoroethylene), poly(ethylene-chlorotrifluoroethylene), poly(tetrafluoroethylene-hexafluoropropylene), poly(tetrafluoroethylene-perfluoroalkyl vinyl ether), poly(tetrafluoroethylene-perfluoromethyl vinyl ether), poly(tetrafluoroethylene-perfluoropropyl vinyl ether),
30 polytetrafluoroethylene, modified polytetrafluoroethylene, polyvinyl fluoride, polyvinylidene fluoride, poly(vinylidene fluoride-hexafluoropropylene), polyethylene, and polypropylene.

11. The fluorinated ion exchange polymer of Claim 10 wherein the perfluoro(alkyl vinyl ether) comprises a perfluoro(propyl vinyl ether) or perfluoro(ethyl vinyl ether).

12. The fluorinated ion exchange polymer of Claim 2 wherein the base polymer comprises a terpolymer of ethylene, tetrafluoroethylene (TFE), and 1 to 10 mole% of a termonomer comprising perfluorobutyl ethylene.

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13. A fluorinated ion exchange polymer membrane comprising a fluorinated ion exchange polymer prepared by grafting a at least one grafting monomer on to at least one base polymer, wherein the grafting monomer comprises structure 1a or 1b:

wherein Z comprises S, SO₂, or POR wherein R comprises a linear or branched perfluoroalkyl group of 1 to 14 carbon atoms optionally containing oxygen or chlorine, an alkyl group of 1 to 8 carbon atoms, an aryl group of 6 to 12 carbon atoms or a substituted aryl group of 6 to 12 carbon atoms;

R_F comprises a linear or branched perfluoroalkene group of 1 to 20 carbon atoms, optionally containing oxygen or chlorine;

Q is chosen from F, -OM, -NH₂, -N(M)SO₂R²_F, and -C(M)(SO₂R²_F)₂, wherein M comprises H, an alkali cation, or ammonium;

R²_F groups comprise alkyl of 1 to 14 carbon atoms which may optionally include ether oxygens or aryl of 6 to 12 carbon atoms where the alkyl or aryl groups may be perfluorinated or partially fluorinated; and n is 1 or 2 for 1a, and n is 1, 2, or 3 for 1b; and wherein the base polymer is a partially or completely fluorinated polymer in film form.

- 14. The fluorinated ion exchange membrane of Claim 13 wherein the base polymer comprises a completely fluorinated polymer.
- 15. The fluorinated ion exchange membrane of Claim 13 wherein the base polymer is chosen from poly(ethylene-tetrafluoroethylene), poly(ethylene-tetrafluoroethylene-termonomer), poly(tetrafluoroethylene-tetr

hexafluoropropylene), poly(tetrafluoroethylene-perfluorovinylether), polytetrafluoroethylene, poly(ethylene-chlorotrifluoroethylene); poly(vinyledene fluoride), and poly(vinylidenefluoride-hexafluoropropylene).

- 16. The fluorinated ion exchange membrane of Claim 15 wherein the base polymer is chosen from poly(ethylene-tetrafluoroethylene-termonomer), poly(tetrafluoroethylene-hexafluoropropylene), poly(tetrafluoroethylene-perfluoropropylvinylether), and poly(vinyledene fluoride).
- 17. The fluorinated ion exchange membrane of Claim 15 wherein the base polymer comprises a terpolymer of ethylene, tetrafluoroethylene (TFE), and 1 to 10 mole% of a termonomer comprising perfluorobutyl ethylene.
 - 18. A grafting process for making the fluorinated ion exchange polymer membrane comprising:
 - (a) forming an monomer composition comprising at least one grafting monomer, in neat form, emulsion form, or solution form, wherein the grafting monomer comprises structure 1a or 1b:

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wherein Z comprises S, SO₂, or POR wherein R comprises a linear or branched perfluoroalkyl group of 1 to 14 carbon atoms optionally containing oxygen or chlorine, an alkyl group of 1 to 8 carbon atoms, an aryl group of 6 to 12 carbon atoms or a substituted aryl group of 6 to 12 carbon atoms;

R_F comprises a linear or branched perfluoroalkene group of 1 to 20 carbon atoms, optionally containing oxygen or chlorine;

Q is chosen from F, -OM, -NH₂, -N(M)SO₂R²_F, and -C(M)(SO₂R²_F)₂, wherein M comprises H, an alkali cation, or ammonium;

R²_F groups comprise alkyl of 1 to 14 carbon atoms which may optionally include ether oxygens or aryl of 6 to 12 carbon atoms where the alkyl or aryl groups may be perfluorinated or partially fluorinated; and

n is 1 or 2 for 1a, and n is 1, 2, or 3 for 1b

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- (b) irradiating at least one base polymer with ionizing radiation, and
- (c) contacting at least one base polymer with the monomer composition from step (a), at a temperature of about 0 °C to about 120 °C for about 0.1 hours to about 500 hours.
 - 19. The process of Claim 18 wherein the at least one base polymer is in film form.
 - 20. The process of Claim 18 wherein steps (b) and (c) are performed simultaneously.
- 10 21. The process of Claim 18 wherein steps (b) and (c) are performed sequentially.
 - 22. The process of Claim 18 wherein Q comprises F.
- 23. The process of Claim 18 wherein R_F is chosen from (CF₂)_q wherein q = 1 to 16, (CF₂)_qOCF₂CF₂ wherein q = 1 to 12, and
 15 (CF₂CF(CF₃)O)_qCF₂CF₂ wherein q = 1 to 6, and R²_F is chosen from methyl, ethyl, propyl, butyl, and phenyl, each of which may be partially fluorinated or perfluorinated.
- 24. The process of Claim 23 wherein R_F is chosen from (CF₂)_q wherein q = 1 to 4; (CF₂)_qOCF₂CF₂ wherein q = 1 to 4; and (CF₂CF(CF₃)O)_qCF₂CF₂ wherein q = 1 to 2, and R²_F is chosen from perfluoromethyl, perfluoroethyl, and perfluorophenyl.
- 25. The process of Claim 18 wherein the grafting monomer further comprises at least one co-monomer chosen from compounds containing single or multiple vinyl groups; at least one monomer having the structure
 25 2 or 3; and mixtures thereof:

wherein Y comprises H; halogen such as Cl, Br, F or I; linear or branched alkyl or perfluoroalkyl groups, wherein the alkyl group comprises C1 to C10 carbon atoms; or a perfluoroalkyl group containing oxygen, chlorine or bromine, and wherein the alkyl group comprises C1 to C10 carbon atoms

26. The process of Claim 25 wherein the compounds containing single or multiple vinyl groups comprise bis(trifluorovinyl)-benzene's of structure 2 or triallyl cyanurate.

27. The process of Claim 25 wherein the substituents Y on comonomer of structure 3 are chosen from hydrogen, chlorine, fluorine, methyl, ethyl, methoxy, perfluoromethyl, perfluoroethyl, perfluorobutyl, perfluoromethoxy, and -CF₂CF(CF₃)OCF₂CF₃.

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- 28. The process of Claim 18 wherein the base polymer comprises a homopolymer or copolymer prepared from non-fluorinated, fluorinated, or perfluorinated monomers.
- 29. The process of Claim 28 wherein the base polymer is chosen from poly(ethylene-tetrafluoroethylene), poly(ethylene-chlorotrifluoroethylene), poly(tetrafluoroethylene-hexafluoropropylene), poly(tetrafluoroethylene-perfluoroalkyl vinyl ether), poly(tetrafluoroethylene-perfluoromethyl vinyl ether), poly(tetrafluoroethylene-perfluoropropyl vinyl ether), polytetrafluoroethylene, modified polytetrafluoroethylene, polyvinyl fluoride, polyvinylidene fluoride, poly(vinylidene fluoride-hexafluoropropylene), polyethylene, and polypropylene.
 - 30. The process of Claim 28 wherein the base polymer comprises a partially or completely fluorinated polymer.
 - 31. The process of Claim 30 wherein the base polymer is chosen from poly(ethylene-tetrafluoroethylene), poly(ethylene-tetrafluoroethylene-tetrafluoroethylene-tetrafluoroethylene-hexafluoropropylene), poly(tetrafluoroethylene-perfluorovinylether), polytetrafluoroethylene, poly(ethylene-chlorotrifluoroethylene); poly(vinyledene fluoride), and poly(vinylidenefluoride-hexafluoropropylene).
 - 32. A catalyst coated membrane comprising a polymer electrolyte membrane having a first surface and a second surface, wherein the polymer electrolyte membrane comprises a fluorinated ion exchange polymer prepared by grafting at least one grafting monomer on to at least one base polymer, wherein the grafting monomer comprises structure 1a or 1b:

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wherein Z comprises S, SO₂, or POR wherein R comprises a linear or branched perfluoroalkyl group of 1 to 14 carbon atoms optionally containing oxygen or chlorine, an alkyl group of 1 to 8 carbon atoms, an aryl group of 6 to 12 carbon atoms or a substituted aryl group of 6 to 12 carbon atoms;

 R_{F} comprises a linear or branched perfluoroalkene group of 1 to 20 carbon atoms, optionally containing oxygen or chlorine;

Q is chosen from F, -OM, -NH₂, -N(M)SO₂R²_F, and -C(M)(SO₂R²_F)₂, wherein M comprises H, an alkali cation, or ammonium;

 R^2_F groups comprise alkyl of 1 to 14 carbon atoms which may optionally include ether oxygens or aryl of 6 to 12 carbon atoms where the alkyl or aryl groups may be perfluorinated or partially fluorinated; and n is 1 or 2 for 1a, and n is 1, 2, or 3 for 1b.

- 33. The catalyst coated membrane of Claim 32 wherein the base polymer is in film form.
- 34. The catalyst coated membrane of Claim 32 further comprising at least one electrode prepared from an electrocatalyst coating composition present on the first and second surfaces of the polymer electrolyte membrane.
- 35. The catalyst coated membrane of Claim 34 wherein the at least one electrode is an anode.
- 36. The catalyst coated membrane of Claim 34 wherein the at least one electrode is a cathode.
 - 37. The catalyst coated membrane of Claim 34 wherein the electrocatalyst coating composition comprises a catalyst and a binder.
 - 38. The catalyst coated membrane of Claim 37 wherein the binder is a perfluorosulfonic acid polymer.
- 39. The catalyst coated membrane of Claim 32 wherein the at least one grafting monomer further comprises at least one co-monomer chosen from compounds containing single or multiple vinyl groups; at least one monomer having the structure 2 or 3; and mixtures thereof:

wherein Y comprises H; halogen such as Cl, Br, F or I; linear or branched alkyl or perfluoroalkyl groups, wherein the alkyl group comprises C1 to C10 carbon atoms; or a perfluoroalkyl group containing oxygen, chlorine or bromine, and wherein the alkyl group comprises C1 to C10 carbon atoms

40. A membrane electrode assembly comprising a polymer electrolyte membrane, having a first surface and a second surface, wherein the polymer electrolyte membrane comprises a fluorinated ion exchange polymer prepared by grafting at least one grafting monomer on to at least one base polymer, wherein the grafting monomer comprises structure 1a or 1b:

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wherein Z comprises S, SO₂, or POR wherein R comprises a linear or branched perfluoroalkyl group of 1 to 14 carbon atoms optionally containing oxygen or chlorine, an alkyl group of 1 to 8 carbon atoms, an aryl group of 6 to 12 carbon atoms or a substituted aryl group of 6 to 12 carbon atoms;

R_F comprises a linear or branched perfluoroalkene group of 1 to 20 carbon atoms, optionally containing oxygen or chlorine;

Q is chosen from F, -OM, -NH₂, -N(M)SO₂R²_F, and -C(M)(SO₂R²_F)₂, wherein M comprises H, an alkali cation, or ammonium;

R²_F groups comprise alkyl of 1 to 14 carbon atoms which may optionally include ether oxygens or aryl of 6 to 12 carbon atoms where the alkyl or aryl groups may be perfluorinated or partially fluorinated; and

n is 1 or 2 for 1a, and n is 1, 2, or 3 for 1b.

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41. The membrane electrode assembly of Claim 40 wherein the base polymer is in film form.

- 42. The membrane electrode assembly of Claim 40 further comprising at least one electrode prepared from an electrocatalyst coating composition present on the first or second surfaces of the membrane.
- 43. The membrane electrode assembly of Claim 42 wherein at least one electrode is an anode.
- 44. The membrane electrode assembly of Claim 42 wherein at least one electrode is a cathode.
 - 45. The membrane electrode assembly of Claim 42 wherein the electrocatalyst coating composition comprises a catalyst and a binder.
 - 46. The membrane electrode assembly of Claim 45 wherein the binder is a perfluorosulfonic acid polymer.
 - 47. The membrane electrode assembly of Claim 40 further comprising at least one gas diffusion backing adjacent at least one electrode present on the polymer electrolyte membrane.
 - 48. The membrane electrode assembly of Claim 40 further comprising at least one gas diffusion electrode present on the first or second surfaces of the membrane, wherein the gas diffusion electrode comprises a gas diffusion backing and an electrode prepared from an electrocatalyst coating composition.
 - 49. The membrane electrode assembly of Claim 40 wherein Q comprises F.
 - 50. The membrane electrode assembly of Claim 40 wherein R_F is chosen from $(CF_2)_q$ wherein q=1 to 16, $(CF_2)_q OCF_2 CF_2$ wherein q=1 to 12, and $(CF_2 CF(CF_3)O)_q CF_2 CF_2$ wherein q=1 to 6, and R^2_F is chosen from methyl, ethyl, propyl, butyl, and phenyl, each of which may be partially fluorinated or perfluorinated.
 - 51. The membrane electrode assembly of Claim 40 wherein the at least one grafting monomer further comprises at least one co-monomer chosen from compounds containing single or multiple vinyl groups; at least one monomer having the structure 2 or 3; and mixtures thereof:

wherein Y comprises H; halogen such as Cl, Br, F or I; linear or branched alkyl or perfluoroalkyl groups, wherein the alkyl group comprises C1 to C10 carbon atoms; or a perfluoroalkyl group containing oxygen, chlorine or bromine, and wherein the alkyl group comprises C1 to C10 carbon atoms

- 52. The membrane electrode assembly of Claim 51 wherein the compounds containing single or multiple vinyl groups are bis(trifluorovinyl)-benzenes of structure 2 or triallyl cyanurate.
- 53. The membrane electrode assembly of Claim 51 wherein the substituents Y on co-monomer of structure 3 are chosen from the group consisting of hydrogen, chlorine, fluorine, methyl, ethyl, methoxy, perfluoromethyl, perfluoroethyl, perfluorobutyl, perfluoromethoxy, and -CF₂CF(CF₃)OCF₂CF₃.

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- 54. The membrane electrode assembly of Claim 41 wherein the at least one base polymer comprises a homopolymer or copolymer prepared from non-fluorinated, fluorinated, or perfluorinated monomers.
- 55. The membrane electrode assembly of Claim 54 wherein the at least one base polymer is chosen from poly(ethylene-tetrafluoroethylene), poly(ethylene-chlorotrifluoroethylene), poly(tetrafluoroethylene-hexafluoropropylene), poly(tetrafluoroethylene-perfluoromethylene-perfluoromethyl vinyl ether), poly(tetrafluoroethylene-perfluoropropyl vinyl ether), poly(tetrafluoroethylene-perfluoropropyl vinyl ether), polytetrafluoroethylene, modified polytetrafluoroethylene, polyvinyl fluoride, polyvinylidene fluoride, poly(vinylidene fluoride-hexafluoropropylene), polyethylene, and polypropylene.
 - 56. The membrane electrode assembly of Claim 54 wherein the at least one base polymer is chosen from poly(ethylene-tetrafluoroethylene), poly(ethylene-tetrafluoroethylene-termonomer), poly(tetrafluoroethylene-hexafluoropropylene), poly(tetrafluoroethylene-perfluorovinylether), polytetrafluoroethylene, poly(ethylene-chlorotrifluoroethylene);

poly(vinyledene fluoride), and poly(vinylidenefluoridehexafluoropropylene).

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- 57. The membrane electrode assembly of Claim 56 wherein the at least one base polymer comprises a terpolymer of ethylene, tetrafluoroethylene (TFE), and 1 to 10 mole% of a perfluorobutyl ethylene.
- 58. The fluorinated ion exchange polymer of Claim 55 wherein the perfluoro(alkyl vinyl ether), comprises perfluoro(propyl vinyl ether) or perfluoro(ethyl vinyl ether).
- 59. The membrane electrode assembly of Claim 54 wherein the at least one base polymer comprises a terpolymer of ethylene, tetrafluoroethylene (TFE), and 1 to 10 mole% of a termonomer such as perfluorobutyl ethylene.
 - 60. An electrochemical cell comprising a membrane electrode assembly, wherein the membrane electrode assembly comprises a polymer electrolyte membrane, having a first surface and a second surface, wherein the polymer electrolyte membrane comprises a fluorinated ion exchange polymer prepared by grafting at least one grafting monomer on to at least one base polymer, wherein the grafting monomer comprises structure 1a or 1b:

wherein Z comprises S, SO₂, or POR wherein R comprises a linear or branched perfluoroalkyl group of 1 to 14 carbon atoms optionally containing oxygen or chlorine, an alkyl group of 1 to 8 carbon atoms, an aryl group of 6 to 12 carbon atoms or a substituted aryl group of 6 to 12 carbon atoms;

R_F comprises a linear or branched perfluoroalkene group of 1 to 20 carbon atoms, optionally containing oxygen or chlorine;

Q is chosen from F, -OM, -NH₂, -N(M)SO₂R²_F, and -C(M)(SO₂R²_F)₂, wherein M comprises H, an alkali cation, or ammonium;

 R^2_F groups comprise alkyl of 1 to 14 carbon atoms which may optionally include ether oxygens or aryl of 6 to 12 carbon atoms where the alkyl or aryl groups may be perfluorinated or partially fluorinated; and n is 1 or 2 for 1a, and n is 1, 2, or 3 for 1b.

- 61. The electrochemical cell of Claim 56 wherein the electrochemical cell is a fuel cell.
- 62. The electrochemical cell of Claim 61 wherein the base polymer is in film form.
- 63. The electrochemical cell of Claim 60 wherein the at lest one grafting monomer further comprises at least one co-monomer chosen from compounds containing single or multiple vinyl groups; at least one monomer having the structure 2 or 3; and mixtures thereof:

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wherein Y comprises H; halogen such as Cl, Br, F or I; linear or branched alkyl or perfluoroalkyl groups, wherein the alkyl group comprises C1 to C10 carbon atoms; or a perfluoroalkyl group containing oxygen, chlorine or bromine, and wherein the alkyl group comprises C1 to C10 carbon atoms

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64. The electrochemical cell of Claim 61 wherein the at lest one grafting monomer further comprises at least one co-monomer chosen from compounds containing single or multiple vinyl groups; at least one monomer having the structure 2 or 3; and mixtures thereof:

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wherein Y comprises H; halogen such as Cl, Br, F or I; linear or branched alkyl or perfluoroalkyl groups, wherein the alkyl group comprises C1 to

C10 carbon atoms; or a perfluoroalkyl group containing oxygen, chlorine or bromine, and wherein the alkyl group comprises C1 to C10 carbon atoms.

- 65. The fuel cell of Claim 61 further comprising at least one electrode prepared from an electrocatalyst containing composition present on the first and second surfaces of the polymer electrolyte membrane.
- 66. The fuel cell of Claim 60 further comprising at least one gas diffusion backing.

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- 67. The fuel cell of Claim 61 further comprising at least one gas diffusion electrode present on the first and second surfaces of the membrane, wherein the gas diffusion electrode comprises a gas diffusion backing and an electrode prepared from an electrocatalyst containing composition.
- 68. The fuel cell of Claim 61 further comprising a means for delivering a fuel to the anode, a means for delivering oxygen to the cathode, a means for connecting the anode and cathode to an external electrical load, hydrogen or methanol in the liquid or gaseous state in contact with the anode, and oxygen in contact with the cathode.
- 69. The fuel cell of Claim 64 further comprising a means for delivering a fuel to the anode, a means for delivering oxygen to the cathode, a means for connecting the anode and cathode to an external electrical load, hydrogen or methanol in the liquid or gaseous state in contact with the anode, and oxygen in contact with the cathode.
 - 70. The fuel cell of Claim 68 wherein the fuel is an alcohol or ether.
 - 71. The fuel cell of Claim 70 wherein the fuel is methanol.
- 72. The fuel cell of Claim 68 wherein the fuel is hydrogen.

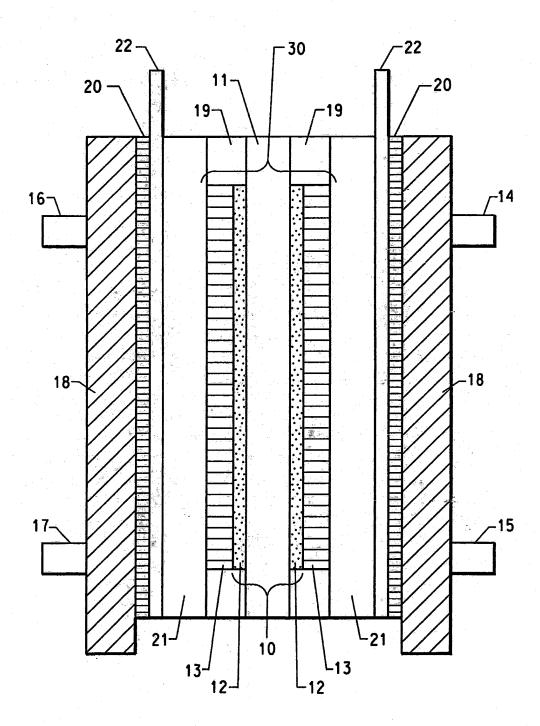


FIG. 1

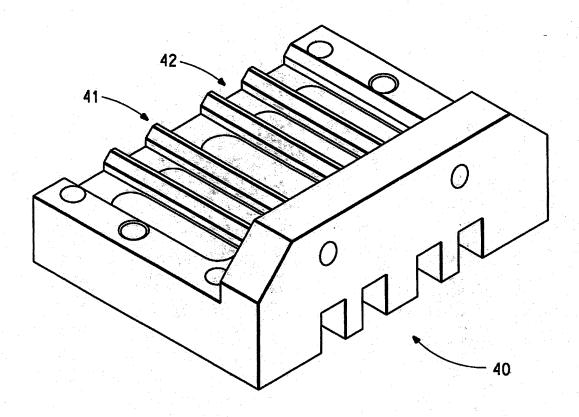


FIG. 2

INTERNATIONAL SEARCH REPORT

International Application No PCT/US2004/020701

A. CLASSIFICATION OF SUBJECT MATTER IPC 7 C08F291/00 C08F291/18 B01D71/78 B01D71/28 C08F259/08 C08F255/02 According to International Patent Classification (IPC) or to both national classification and IPC **B. FIELDS SEARCHED** Minimum documentation searched (classification system followed by classification symbols) CO8F B01D C08J IPC 7 Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched Electronic data base consulted during the international search (name of data base and, where practical, search terms used) EPO-Internal, WPI Data, PAJ C. DOCUMENTS CONSIDERED TO BE RELEVANT Relevant to claim No. Citation of document, with Indication, where appropriate, of the relevant passages Category ° US 6 359 019 B1 (STONE CHARLES ET AL) 1-12 X 19 March 2002 (2002-03-19) column 1, lines 5-22 column 2, line 25 - column 6, line 46; claims 1-39 WO 01/58576 A (BALLARD POWER SYSTEMS INC; 1-6,9-11 Χ STONE, CHARLES; STECK, ALFRED, E) 16 August 2001 (2001-08-16) page 1, lines 5-29 page 8, lines 20-26 page 12, lines 19-21 page 4, line 20 - page 12, line 21 page 13, line 19 - page 20, line 30; claims 1-62 Further documents are listed in the continuation of box C. Patent family members are listed in annex. Special categories of cited documents: "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the "A" document defining the general state of the art which is not considered to be of particular relevance "E" earlier document but published on or after the international "X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone filing date "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) "Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art. "O" document referring to an oral disclosure, use, exhibition or "P" document published prior to the international filing date but later than the priority date claimed "&" document member of the same patent family Date of mailing of the international search report Date of the actual completion of the international search 0'6 OCT 2005 24 May 2005 Authorized officer Name and mailing address of the ISA European Patent Office, P.B. 5818 Patentiaan 2 NL - 2280 HV Rijswijk Tel. (+31-70) 340-2040, Tx. 31 651 epo nl, Fax: (+31-70) 340-3016 Hammond, A

INTERNATIONAL SEARCH REPORT

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International application No. PCT/US2004/020701

INTERNATIONAL SEARCH REPORT

Box II Observations where certain claims were found unsearchable (Continuation of Item 2 of first sheet)
This International Search Report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:
1. Claims Nos.: because they relate to subject matter not required to be searched by this Authority, namely:
2. Claims Nos.: because they relate to parts of the International Application that do not comply with the prescribed requirements to such an extent that no meaningful International Search can be carried out, specifically:
3. Claims Nos.: because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).
Box III Observations where unity of invention is lacking (Continuation of item 3 of first sheet)
This International Searching Authority found multiple inventions in this international application, as follows:
see additional sheet
1. As all required additional search fees were timely paid by the applicant, this International Search Report covers all searchable claims.
2. As all searchable claims could be searched without effort justifying an additional fee, this Authority did not invite payment of any additional fee.
As only some of the required additional search fees were timely paid by the applicant, this International Search Report covers only those claims for which fees were paid, specifically claims Nos.:
4. X No required additional search fees were timely paid by the applicant. Consequently, this international Search Report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:
1 - 12
Remark on Protest The additional search fees were accompanied by the applicant's protest.
No protest accompanied the payment of additional search fees.

FURTHER INFORMATION CONTINUED FROM PCT/ISA/ 210

This International Searching Authority found multiple (groups of) inventions in this international application, as follows:

1. claims: 1-12

A fluorinated polymer suitable for ion exchange prepared by grafting at least one grafting monomer of formulae 1a or 1b, onto at least one base polymer as described in the application claim 1.

2. claims: 13-17

An independent ion exchange membrane which is not dependent on any preceeding application claim. The said membrane comprising fluorinated polymer as described in application claim 13.

3. claims: 18-31

An independent grafting process as described in application claim 18, which is not dependent on any previous application claim.

4. claims: 32-39

An independent catalyst coated membrane comprising various surfaces as described in the application claim 32, and not dependent on any previous application claim.

5. claims: 40-59

An independent membrane electrode assembly as described in the application claim 40, and not dependent on any previous application claim.

6. claims: 60-72

An independent electrochemical cell as described in the application claim 60, which is not dependent on any previous application claim.

INTERNATIONAL SEARCH REPORT

International Application No
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C.(Continu	ILÍON) DOCUMENTS CONSIDERED TO BE RELEVANT		4444
Category °	Citation of document, with indication, where appropriate, of the relevant passages		Relevant to claim No.
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